

## CLAIM AMENDMENTS

Amended claims: 1-10 and canceled claim 11.

1. (Currently Amended) A process for making multiple grades of base oil products, wherein said process comprises ~~Process to prepare simultaneously two or more base oil grades and middle distillates from a mineral crude derived feed, in particular a de-asphalted oil or a vacuum distillate feed or their mixtures, by performing~~ the following steps:

- (a) hydrocracking ~~a~~ the mineral crude derived feed, thereby obtaining an effluent;
  - (b) distilling distillation of the effluent as obtained in step (a) into at least one or more middle distillates product and a full range residue boiling substantially above 340 °C[.];
  - (c) catalytically dewaxing the full range residue by contacting the full range residue with a dewaxing catalyst comprising a zeolite of the MTW type and a Group VIII metal, thereby obtaining a dewaxed oil;
  - (d) isolating by means of distillation two or more base oil grades from the dewaxed oil obtained in step (c); and
  - (e) isolating a dewaxed gas oil from the dewaxed[[-]]oil obtained in step (c);
- wherein the dewaxed oil as obtained in step (c) comprises between 10 and 40 wt% of a dewaxed heavy gas oil boiling for more than 70 wt% between 370 and 400 °C.

2. (Currently Amended) The process ~~Process~~ according to claim 1, wherein more than 20 wt% of the mineral crude derived feed to step (a) boils above 470 °C.

3. (Currently Amended) The process ~~Process~~ according to claim ~~1~~ or 2, wherein a fraction of comprising the dewaxed gas oil is recycled to step (b) to be mixed with the effluent before distilling thereof ~~obtain a mixture of hydrocracked and dewaxed gas oil.~~

4. (Currently Amended) The process ~~Process~~ according to claim 3, ~~any one of claims 1-3~~, wherein between from 0 and to 15 wt% of the full range residue as obtained in step (b) is recycled to step (a) to be mixed with the mineral crude derived feed before hydrocracking thereof.

5. (Currently Amended)     The process ~~Process~~ according to claim 4, further comprising adding any one of claims 1-4, wherein the feed to step (e) also comprises a Fischer-Tropsch derived partly isomerised paraffin fraction to the full range residue prior to catalytically dewaxing.
6. (Currently Amended)     The process ~~Process~~ according to any one of claim[[s 1-]]5, wherein the ~~effluent~~ dewaxed oil of step (c) is subjected to an additional hydrofinishing step.
7. (Currently Amended)     The process ~~Process~~ according to claim 6, wherein the hydrogen partial pressure in step (c) is greater than 100 bars.
8. (Currently Amended)     The process ~~Process~~ according to claims ~~6-7~~, wherein the base oil grades obtained in step (d) each ~~comprises of~~ more than 95 wt% of saturates and have a viscosity index of between 95 and 120.
9. (Currently Amended)     A dewaxed ~~Dewaxed~~ gas oil made by the process of claim 1 obtainable according to step (e) of any one of the preceding claims 1-8.
10. (Currently Amended)     A dewaxed ~~Dewaxed~~ gas oil according to claim 9, wherein the gas oil has an aromatic content of below 0.1 mmol/100 grams, a sulphur content of below 10 ppm and a pour point of below -30 °C.
11. (Canceled)